VCS Tank & Test Cart HAZOP

Study approach: Deviation by Deviation Table Drawing No.:

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Node:	VCS Tank	

Intent: ____Store liquid and supply gaseous hydrogen at 20 psi______

Guide Word	Deviation	Causes	Consequences	Safeguards	Recommendations
High Flow	Too much flow from regulator (higher than FC can use)	Heater overpower, failure of insulation, oversupply from dewar, See high temperature.	See high pressure.	Heater control system, ortho-para converter, designed for multiple boiloff rates, low-pressure fills from dewar.	Quantify nominal flow rate range for FC.
High Flow	Too much flow for PRD.	Same as above.	Rupture.	Design, test, and validate PRD operation. Dual-redundant PRDs.	Determine max flow rate of single PRD.
High Flow	Too much flow for tank passageways	Oversupply from dewar to hot tank, obstruction to passageway.	Rupture.	Tank passageway designed to pressure relief standards, low pressure fills.	Determine max LH2 flow and evaporation rate (hot tank) and where/what will choke first.
High Flow	Too much flow for 1/4" Valve TN709	Same as above	See high pressure.	Designed to pressure relief standards, low pressure fills.	Test.
Low/no flow	Too little flow from regulator (lower than FC needs)	Obstruction/blockage, damage, changed heater setpoint or broken heater, low pressure.	Unable to supply adequate hydrogen to FC, see high pressure.	Routine maintenance and operation.	Verify advertised temperature operating range of components.

Guide Word	Deviation	Causes	Consequences	Safeguards	Recommendations
Low/no flow	Too little flow from PRDs	Obstruction/blockage, see high flow, heater setpoint, choked flow/high pressure, poor purge, see impurity.	See high pressure. Rupture, tank fragment blockage.	Routine maintenance and operation.	Develop maintenance log/schedule.
Low/no flow	Too little flow through passageways	Obstruction/blockage (print powder or catalyst, poor purge), heater setpoint, choked flow/high pressure.	Rupture, see high pressure.	Ensure pure gas and proper purge. Test for blockage at room temperature.	Investigate whether gas sampling is required.
Low/no flow	Too little flow through 1/4" valve TN709	Obstruction/blockage (print powder or catalyst, poor purge), heater setpoint, choked flow/high pressure.	Rupture, see high pressure.	Visually inspect and manually operate prior to fill.	Test.
Low/no flow	Too little flow through quick connect	Obstruction/blockage, heater setpoint, choked flow/high pressure.	Unable to fill or operate	Cap when not in operation.	
High level	Overfill of tank resulting in liquid within vapor passageway	Overfill of 90% of tank capacity.	Failure to shutoff liquid fill.	Tank passageway will naturally boil outer shell to prevent high level.	

High	Overpressure	PRD failure,	Overpressure above	Proper purge, pure gases,	Will consider new
Pressure	in liquid	obstruction/blockage,	MAWP, see high	liquefier condenses	pressure tap.
(liquid	space	heater overpower,	flow.	impurities, scope if	
space)	30 <p<45 psig<="" td=""><td>failed insulation,</td><td></td><td>refurbishing/recertification.</td><td></td></p<45>	failed insulation,		refurbishing/recertification.	
High	Overpressure	PRD failure,	Rupture	Proper purge, pure gases,	Will consider new
Pressure	in liquid	obstruction/blockage,		liquefier condenses	pressure tap.
(liquid	space P>45	heater overpower,		impurities, scope if	
space)	psig	failed insulation,		refurbishing/recertification.	

Guide Word	Deviation	Causes	Consequences	Safeguards	Recommendations
High	P>2 psig	Leak	Loss of insulation,	Cryopumping, aerogel	Determine nominal
Pressure	delta from		rupture	insulation,	pressure values for
(insulation)	liquid space				insulation space. PRD
					device for insulation
					layer.
High	Overpressure	PRD failure,	Overpressure above	Proper purge, pure gases,	
Pressure	30 <p<45 psig<="" td=""><td>obstruction/blockage,</td><td>MAWP, see high</td><td>liquefier condenses</td><td></td></p<45>	obstruction/blockage,	MAWP, see high	liquefier condenses	
(vapor		heater overpower,	flow.	impurities, scope if	
passageways)		failed insulation,		refurbishing/recertification.	
High	Overpressure	PRD failure,	Rupture	Proper purge, pure gases,	
Pressure	P>45 psig	obstruction/blockage,		liquefier condenses	
(vapor		heater overpower,		impurities, scope if	
passageways)		failed insulation,		refurbishing/recertification.	
Low Pressure	P<20 psig	Heater control loop failure, leak,	FC Failure	Precheck heat control loop prior to operation.	
Low pressure	P<4 psig	Improper storage, left open vent valve,	Impurities, rupture,	Follow proper storage guidelines	Write operating manual for tank storage.

		improper purge procedure.			
High Temperature	T>350F	Fire, heater run away in empty tank	Melting, leak, rupture, deflagration ∂	Follow standards and procedures to minimize risk	Consider bonding temp sensor to heater to monitor output with feedback loop to shutoff heater above 40C
Low Temperature	T< -40C	Flow rate too high, operating tank in cold conditions, liquid level too high flowing in to vapor channels	Possible leakage out of non-cryo rated seals	Follow operating manual	Confirm lower temp limit for polymer seals

Guide Word	Deviation	Causes	Consequences	Safeguards	Recommendations
High	>0.001%	Impurities in	Blockage of vapor	Proper purge, pure gases,	Investigate if tank bake
concentration	for gas	hydrogen stream	passages & PRDs, see	liquefier condenses	out process for moisture
in vapor	impurities		high pressure	impurities, scope if	removal in nylon is
passages				refurbishing/recertification.	required
				Follow operating/storage	
				procedures for fuel	
				connection	
High Power	Heater	Heater control	Heater lead wire		Investigate if fuse can be
	power >	loop failure	burns out – loss of		utilized on control board,
	10W		heater, unable to		or transistorized switch to
			operate		meet Div1 Class1 rating
Leak	Leak from	Incomplete seal	Gentle h2 stream,		Design fluid tight cap
	LH2	after valve closure	unable to build		
	disconnect		pressure in tank,		
			deflagration		
Leak	Fluid	Improper	Small H2 leak	Leak check	
	plumbing	installation,			
	component	thermal			
	leaks	contraction,			
		thermal cycling,			
		vibration			
Leak	Tank wall	Thermal cycling,	Fire from leak		
	crack	impact, H2 fire			
		from adjacent leak			
Rupture	Tank wall	Thermal cycling,	Deflagration,	Transportation case,	
		impact, H2 fire	detonation	secured to test stand	
		from adjacent			
		leak, see high			
		pressure, see low			

		pressure, crushing			
		in mount device			
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Guide Word	Deviation	Causes	Consequences	Safeguards	Recommendations
No	Manual	Improper	Valve won't open –		
movement	vent valve	installation or	cannot fill; valve		
	handle	operation	won't close – cannot		
	departs		fly		
Unintended	Regulator	Vibration	Change in flow	Ensure jam nut is secure	
movement	set point		pressure to FC		
	screw				
Unintended	Quick	Vibration,	H2 leak, low pressure		Future installation of
movement	connect	improper	in tank, deflagration		aircraft safetywire
	hold-down	installation			
	screws				
Unintended	PRD	Vibration,	Misdirected flow into		Future installation of
movement	collector	improper	electric motor		aircraft safetywire
	screws	installation			
Unintended	Control	Vibration,	Disconnect from tank		Future installation of
movement	board	improper	temp sensors and		aircraft safetywire
	screws	installation	heater, loss of data		
			flow and ability to		
			control heater		