

Last time we ~~balanced~~ balanced entropy on open systems. Today we continue our 2nd law analysis of open systems → this will allow us to define meaningful efficiencies for them.

Turbine: Find turbine power & its efficiency
 $T_1 = 1000 \text{ K}$, $P_1 = 400 \text{ kPa}$
 air $\dot{m} = 0.25 \text{ kg/s}$

Open System Mass Balance: $\dot{m}_{in} = \dot{m}_{out} + \frac{d m_{stored}}{dt}$

Energy Balance: $\dot{E}_{in} = \dot{E}_{out} + \frac{dE_{stored}}{dt}$ (0/s)

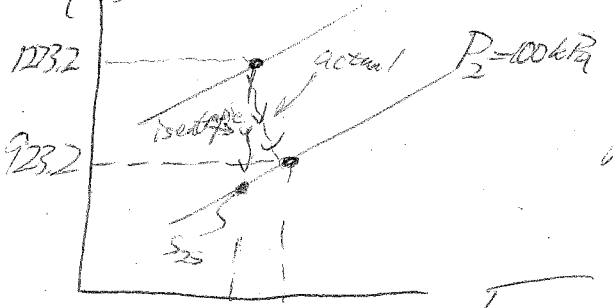
(2) $T_2 = 650 \text{ °C}$, $P_2 = 100 \text{ kPa}$

$$\underbrace{\dot{Q}_{in}}_{0 \text{ (adiabatic)}} + \underbrace{\dot{W}_{in}}_{0} + \dot{m}_{in} \left(h_{in} + \frac{V_{in}^2}{2} + g z_{in} \right) = \underbrace{\dot{Q}_{out}}_{0} + \underbrace{\dot{W}_{out}}_{\text{work}} + \dot{m}_{out} \left(h_{out} + \frac{V_{out}^2}{2} + g z_{out} \right)$$

(Kinetic & PE, KE negligible)
(adiabatic)

$\dot{m}_{in} h_{in} = \dot{W}_{out} + \dot{m}_{out} h_{out} \Rightarrow \dot{W}_{out} = \dot{m} (h_{in} - h_{out})$ ← assume ideal gas constant c_p

$\dot{W}_{out} = \dot{m} c_p (T_{in} - T_{out}) \Rightarrow \frac{0.25 \text{ kg}}{\text{s}} \cdot 1005 \frac{\text{J}}{\text{kg} \cdot \text{K}} \cdot (1233.2 - 923.2) \text{ K} \Rightarrow \dot{W}_{out} = 8,743.75 \text{ W}$



T-h & T-s diagrams are more useful in industry. Why? Entropy is a description of efficiency & Entropy a measure of work possible.

Entropy Balance: $\dot{S}_{in} + \dot{S}_{Gen} = \dot{S}_{out} + \frac{dS_{stored}}{dt}$

$\dot{m} S_{in} + \dot{S}_{Gen} = \dot{m} S_{out} \Rightarrow \dot{S}_{Gen} = \dot{m} (s_{out} - s_{in}) \Rightarrow \dot{S}_{Gen} = \dot{m} \left[c_p \ln \left(\frac{T_{out}}{T_{in}} \right) - R \ln \left(\frac{P_{out}}{P_{in}} \right) \right]$

$\dot{S}_{Gen} = \frac{0.25 \text{ kg}}{\text{s}} \left[\frac{1005 \text{ J}}{\text{kg} \cdot \text{K}} \ln \left(\frac{923.2}{1233.2} \right) - 287 \frac{\text{J}}{\text{kg} \cdot \text{K}} \ln \left(\frac{100}{400} \right) \right] \Rightarrow \dot{S}_{Gen} = 18.74 \frac{\text{W}}{\text{K}}$

$S_2 > S_1$
just the figure

19.2 ME301 FDD

But how good is the turbine? How do we define its efficiency?

What's the best we could do? \Rightarrow Reversible turbine $S_2 = S_1$

Compare this to actual S_2

\Rightarrow 2 ways to define efficiency

1) System \rightarrow $\frac{\text{What you want}}{\text{What you pay for}}$
 approach used for heat engines, refrigerators, heat pumps. Sometimes called 1st Law efficiency.

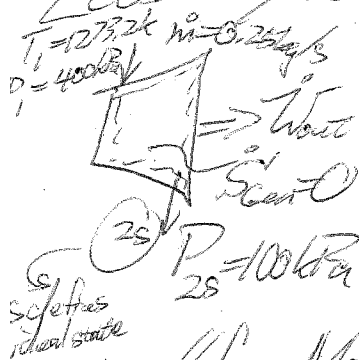
2) Component \rightarrow $\frac{\text{What you got} \rightarrow \text{Actual}}{\text{What you could've} \rightarrow \text{Ideal}}$
 approach used for turbines, compressors, etc... any component. Sometimes called 2nd Law efficiency.

Turbine Efficiency: $\eta = \frac{W_{\text{actual}}}{W_{\text{ideal}}}$
 actual turbine produced 8,938 W
 power produced by a reversible turbine that does the same job.

In limit of $\Delta P \rightarrow 0$, Δh additive: $\eta = \frac{h_1 - h_2}{h_1 - h_{2s}}$

What do I mean by the same job?
 1) receives same fluid @ same inlet conditions
 2) exhausts to the same exit pressure

Let's analyze the reversible turbine that does the same job.



Whenever you analyze a reversible device it's a good idea to start with an entropy balance / 2nd law.

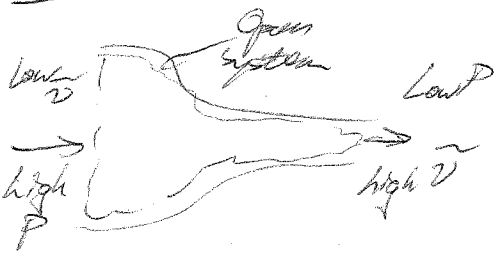
Entropy Balance: $\dot{S}_{in} + \dot{S}_{gen} = \dot{S}_{out} + \frac{dS_{cv}}{dt}$
 (reversible) $\Rightarrow \dot{S}_{in} = \dot{S}_{out} \Rightarrow \dot{m}_1 s_1 = \dot{m}_2 s_2$

recall from Monday: $\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma}{\gamma-1}} \Rightarrow T_2 = 1273.2k \left(\frac{100}{400}\right)^{\frac{1.4}{0.4}} = 856.8k$

Energy Balance: $\dot{E}_{in} = \dot{E}_{out} \Rightarrow \dot{W}_{out} = \dot{m} c_p (T_1 - T_2) = \frac{0.25 \text{ kg/s} \cdot 1005 \text{ J/kgK} \cdot (1273.2 - 856.8) \text{ K}}{19} = 104,600 \text{ W}$

$\eta = \frac{8,938 \text{ W}}{104,600 \text{ W}} \Rightarrow \eta_{\text{turbine}} = 0.841 = 84.1\% \text{ efficient}$

Nozzle: What is the purpose of a nozzle? \rightarrow create exit stream with high v .



So what's the logical definition of a nozzle?
Actual relative to best you can do

$$\eta_{nozzle} = \frac{\frac{1}{2} v_2^2}{\frac{1}{2} v_{2s}^2} \rightarrow \text{actual kinetic energy of exit stream}$$

\rightarrow kinetic energy of exit stream produced by a reversible nozzle that does the same job

1) Same inlet state conditions
2) exhausts to same exit pressure

Energy Balance: $\dot{E}_{in} = \dot{E}_{out} + \frac{dE_{stored}}{dt}$

$$\dot{m} \left(h_{in} + \frac{v_{in}^2}{2} \right) = \dot{m} \left(h_{out} + \frac{v_{out}^2}{2} \right)$$

(adiabatic) (steady)

$\dot{m}_{in} = \dot{m}_{out}$

$$h_{in} + \frac{v_{in}^2}{2} = h_{out} + \frac{v_{out}^2}{2}$$

$$h_{in} - h_{out} = \frac{v_{out}^2}{2}$$

actual

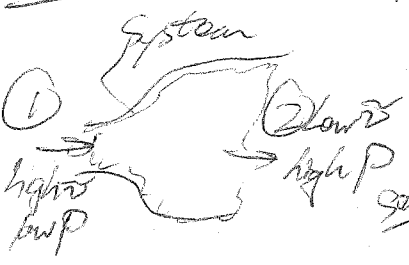
$$h_1 - h_{2s} = \frac{v_{2s}^2}{2}$$

$$\eta_{nozzle} = \frac{h_1 - h_2}{h_1 - h_{2s}}$$

\leftarrow for adiabatic nozzle with no ΔPE

This means if you have the nozzle efficiency, inlet conditions, & exit pressure, you can solve for the final state! Example 7.6

Diffuser: Purpose: Increase in Pressure $P_2 > P_1 \leftarrow$ could also done Velocity



$$\eta_{diff} = \frac{P_2 - P_1}{P_{2s} - P_1} \leftarrow \text{actual } \Delta P$$

\leftarrow ideal ΔP doing same job

1) Same inlet conditions, 2) Same exit velocity

